

## Claims:

264689

1 A precipitated silica, characterized by

BET surface area	170 – 380 m <sup>2</sup> /g
CTAB surface area	≥ 170 m <sup>2</sup> /g
DBP number	305 – 400 g/(100 g)
Sears number V <sub>2</sub>	23 – 35 ml/(5 g).

2. The precipitated silica as claimed in Claim 1,

characterized by the fact that

the CTAB surface area is maximum 300 m<sup>2</sup>/g.

3. The precipitated silica as claimed in any one of Claims 1 or 2,

characterized by the fact that

the precipitated silica has a WK coefficient of ≤ 3.4 (ratio of the peak height of particles that are not decomposed by ultrasound in the size range of 1.0 – 100 μm to the peak height of the decomposed particles in the size range of < 1.0 μm).

4. Precipitated silicas as claimed in any one of Claims 1 to 3,

characterized by the fact that

their surface areas are modified with organosilanes of Formula I to III:



or



with the following meanings

B: -SCN, -SH, -Cl, -NH<sub>2</sub>, -OC(O)CHCH<sub>2</sub>, -OC(O)C(CH<sub>3</sub>)CH<sub>2</sub> (if q = 1) or S<sub>w</sub>- (if q = 2), whereby B is chemically bonded to Alk,

R and R<sup>1</sup>: an aliphatic, olefinic, aromatic or aryl aromatic radical with 2 to 30 C atoms, which can optionally be substituted by the following groups: hydroxyl, amino, alcoholate, cyanide, thiocyanide, halogen, sulfonic acid, sulfonic acid ester, thiol, benzoic acid, benzoic acid ester, carbonic acid, carbonic acid ester,

acrylate, methacrylate, organosilane radical, where R and R<sup>1</sup> can have an identical or different meaning or substitution,

n: 0, 1 or 2,

Alk: a divalent unbranched or branched hydrocarbon radical with 1 to 6 carbon atoms,

m: 0 or 1,

Ar: an aryl radical with 6 to 12 C atoms, preferably 6 C atoms, which can be substituted by the following groups: hydroxyl, amino, alcoholate, cyanide, thiocyanide, halogen, sulfonic acid, sulfonic acid ester, thiol, benzoic acid, benzoic acid ester, carbonic acid, carbonic acid ester, acrylate, methacrylate, organosilane radical,

p: 0 or 1 with the proviso that p and n do not simultaneously mean 0,

q: 1 or 2,

w: a number from 2 to 8,

r: 1, 2 or 3, with the proviso that  $r + n + m + p = 4$ ,

Alkyl: a monovalent unbranched or branched saturated hydrocarbon radical with 1 to 20 carbon atoms, preferably 2 to 8 carbon atoms,

Alkenyl: a monovalent unbranched or branched unsaturated hydrocarbon radical with 2 to 20 carbon atoms, preferably 2 to 8 carbon atoms.

5. A process for manufacture of a precipitated silica with a

BET surface area 170 – 380 m<sup>2</sup>/g

CTAB surface area  $\geq 170$  m<sup>2</sup>/g

DBP number 305 – 400 g/(100 g)

Sears number V<sub>2</sub> 23 – 35 ml/(5 g)

where

a) an aqueous solution of an alkali or alkaline-earth silicate and/or an organic and/or inorganic base with pH  $\geq 9$  is present

b) water glass and an acidifier are metered into this solution with stirring at 55 – 95 °C for 10 – 120 minutes simultaneously,

c) metering is stopped for 30 – 90 minutes while the temperature is maintained, and

d) water glass and acidifier are metered into this solution with stirring at this temperature

for 20 -120 minutes, simultaneously

- e) acidified with acidifier to a pH value of approx. 3.5 and
- f) filtered and dried.

5 6. The process as claimed in Claim 5,

characterized by the fact that

the acidifier and/or the water glass in steps b) and d) have the same concentration or metering rate.

10 7. The process as claimed in Claim 5,

characterized by the fact that

the acidifier and/or the water glass in steps b) and d) have a different concentration or metering rate.

15 8. The process as claimed in Claim 7,

characterized by the fact that

with the same concentration of acidifier and/or water glass in steps b) and d) their metering rate in step d) is 125 - 140 % of the metering rate in step b).

20 9. The process as claimed in any one of Claims 5 to 8,

characterized by the fact that

for the drying process an air-lift drier, a spray drier, a rack drier, a conveyor drier, a rotary drier, a flash drier, a spin flash drier, or a nozzle drier is used.

25 10. The process as claimed in Claim 5 to 9,

characterized by the fact that

after the drying process a granulation process is carried out with a roller compactor.

11. The process as claimed in any one of Claims 5 to 10,

30 characterized by the fact that

during steps b) and/or d) an organic or inorganic salt is added.

12. The process as claimed in any one of Claims 5 to 11,  
characterized by the fact that  
the granulated or ungranulated precipitated silicas are modified with organosilanes in  
mixtures of 0.5 to 50 parts, relative to 100 parts precipitated silica, in particular 1 to 15  
5 parts, relative to 100 parts precipitated silica, where the reaction between precipitated silica  
and organosilane is carried out during production of the mixture (in situ) or outside of  
production by spraying and subsequent tempering of the mixture, or by mixing of the  
organosilane and the silica suspension with subsequent drying and tempering.
- 10 13. Elastomer mixtures, vulcanizable rubber mixtures and vulcanizates, containing the  
precipitated silica as claimed in any one of Claims 1 to 4.
14. Tires, containing precipitated silica as claimed in any one of Claims 1 to 4.
- 15 15. Tires for utility vehicles, containing precipitated silica as claimed in any one of Claims 1 to  
4.
16. Motor cycle tires, containing precipitated silica as claimed in any one of Claims 1 to 4.
- 20 17. Tires for high speed vehicles, containing precipitated silica as claimed in any one of Claims  
1 to 4.